

Cite this: *J. Mater. Chem. A*, 2014, 2, 12888

## Acetoacetanilide-functionalized Fe<sub>3</sub>O<sub>4</sub> nanoparticles for selective and cyclic removal of Pb<sup>2+</sup> ions from different charged wastewaters†

R. K. Sharma,<sup>\*a</sup> Aditi Puri,<sup>a</sup> Yukti Monga<sup>a</sup> and Alok Adholeya<sup>b</sup>

Efficient, selective and reusable acetoacetanilide-functionalized Fe<sub>3</sub>O<sub>4</sub> nanoparticles were developed for the first time for the removal of Pb<sup>2+</sup> ions. A comprehensive characterization of the functionalized nanoparticles, at different levels of synthesis, was carried out by TEM, EDS, XRD, SEM, FT-IR and VSM. The adsorption equilibrium obeyed the Langmuir isotherm model with a maximum enrichment capacity of 392.2 mg g<sup>-1</sup> at 318 K. Pb<sup>2+</sup> ions showed quick removal, and the adsorption rate followed pseudo-second-order kinetics. In addition, isotherm and kinetic studies suggested that the adsorption process is controlled by chemical adsorption, involving the complexation of metal ions with the functional groups present on the surface of the functionalized nanoparticles. The thermodynamic analysis revealed that the analyte adsorption is spontaneous, endothermic and energetically driven in nature. Because the superparamagnetism of the Fe<sub>3</sub>O<sub>4</sub> nanoparticles as the magnetic core and silica coat serve as a protective shell, the adsorbent was easily separated and effectively recycled without significant deterioration in its original performance for at least 10 continuous usages. Furthermore, the proposed environmentally benign analytical process was successfully applied for the selective recovery of Pb<sup>2+</sup> ions from different charged wastewaters.

Received 14th April 2014  
Accepted 10th June 2014

DOI: 10.1039/c4ta01815j

[www.rsc.org/MaterialsA](http://www.rsc.org/MaterialsA)

### Introduction

There is no doubt that industrialization has given a fascinating outlook to society. However, its accelerated pace without commensurate safeguard mechanisms has led to insidious consequences. The failure of this unregulated growth can be observed by the current alarming rates of metal inputs, which has pushed humanity towards environmental and health complexities.<sup>1</sup> Besides this, it has caused an excessive depletion of resources and raised a key concern regarding their availability in the near future. It is predicted that if the current rate of exhaustion continues, we will soon become resource deficit.<sup>2,3</sup> For example, owing to its wide usage with modern technology and industries, lead is one of the most valuable commodities in the present scenario.<sup>4,5</sup> The seemingly valuable properties of this metal have given profitable directions to popular professional sectors, but simultaneously, the current practice rate and urban runoff have resulted in large reserve depletion and environmental disposal in an inaccessible manner. Moreover, its

excessive deposition in various ecological compartments is pushing modern society towards health-related complications, as the metal finds no basic role in the orderly continuation of life.<sup>6,7</sup>

So far, adsorption, membrane separation technology, ion exchange, chemical treatment and electrochemical methods have been employed for the removal of Pb<sup>2+</sup> ions.<sup>1</sup> Among them, adsorption is one of the best available technologies due to its convenient operation process, wide applicability, high efficiency, low energy requirement and cost effectiveness.<sup>7,8</sup> In this perspective, nano-sized materials have nowadays gained much attention because of their unique properties like high surface areas, enhanced active sites and excellent sorption capacities.<sup>9</sup> Bayazit and Inci investigated the adsorption of Pb<sup>2+</sup> on carbon nanotubes oxidized by different methods.<sup>10</sup> In other studies, the adsorptive performance of polymer-based graphene oxide nanocomposites<sup>1</sup> and graphene oxide nanosheets<sup>11</sup> towards Pb<sup>2+</sup> ions were explored. Though the sorption efficiency of the adsorbents was remarkably high; however, their profitable utilization is hindered due to drawbacks like cumbersome synthesis and separation strategy, secondary waste generation, and lack of stability and reusability.

On the other hand, silica-coated iron oxide based nanomaterials have paved the way for their widespread acceptance owing to their ease of separation, environmentally benign and inexpensive nature of the embedded core, repetitive use, outstanding chemical and mechanical stability endowed by impenetrable protective layer and large specific surface area.<sup>12-14</sup>

<sup>a</sup>Green Chemistry Network Centre, Department of Chemistry, University of Delhi, Delhi-110007, India. E-mail: rksharmagreenchem@hotmail.com; Fax: +91-011-27666250; Tel: +91-011-27666250

<sup>b</sup>Biotechnology and Management of Bioresources Division, The Energy and Resource Institute, New Delhi-110003, India. E-mail: aloka@teri.res.in

† Electronic supplementary information (ESI) available. See DOI: 10.1039/c4ta01815j

Furthermore, these magnetically responsive nanoparticles allow simple and facile recovery and recycling of the metals, which is deemed an essential feature to close the resource/waste loop.<sup>15</sup> Therefore, fabrication of these nanomaterials is currently undergoing exciting developments with increasing achievements for Pb<sup>2+</sup> adsorption. The research group of Zhang reported silica-based core-shell nanomaterial prepared *via* a controllable sol-gel process as an efficient adsorbent for Pb<sup>2+</sup> removal.<sup>16</sup> Similarly, Ren *et al.* synthesized magnetic EDTA-modified chitosan/SiO<sub>2</sub>/Fe<sub>3</sub>O<sub>4</sub> nanoparticles with enhanced reusable characteristics.<sup>17</sup> However, these functionalized nanoadsorbents are nonspecific and exhibit low selectivity, which is one of the major challenges in the field of adsorption and is generally limited to ion-imprinted polymers. Cui *et al.* prepared well-defined surface ion-imprinted magnetic microspheres, which displayed selective binding capability for Pb<sup>2+</sup> ions.<sup>18</sup> Likewise, magnetic ion-imprinted polymer (Fe<sub>3</sub>O<sub>4</sub>@SiO<sub>2</sub>-IIP) synthesized by Guo *et al.* showed exclusive selectivity for Pb<sup>2+</sup>.<sup>19</sup> However, from a practical point of view, very low uptake capacities limit their application. Very recently, Chen *et al.* reported double silica layer structured magnetic microspheres for the selective recognition of Pb<sup>2+</sup> using host guest chemistry, but the material suffers from low adsorption capacity and high equilibration time for metal removal. Besides, it could not be reutilized for more than three successive adsorption-desorption cycles.<sup>20</sup> Hence, there is an urgency to develop highly stable functionalized magnetic nanoparticles, which can offer opportunities to reduce energy usage, minimize waste disposal and conserve resources *via* a convenient, efficient, selective and repetitive recovery of Pb<sup>2+</sup> ions.

## Experimental section

### Motivation and strategy

Considering the scarcity of sustainable methods integrating efficiency, selectivity and reusability on a single platform, in the present study, we report novel acetoacetanilide-functionalized Fe<sub>3</sub>O<sub>4</sub> nanoparticles for the removal of Pb<sup>2+</sup> ions from different charged wastewaters including mycorrhizal-treated fly ash. Though various ligands have been used for the surface modifications of nanoparticles to improve their sorption capacity and selectivity,<sup>17,21</sup> no studies have, to date, explored the possibility of using acetoacetanilide (AAA) as an organo-substituent for metal removal. In fact, based on its environmental fate and eco-toxicological properties, AAA is nontoxic to the aquatic environment and can be incorporated easily for the desired purpose. Moreover, considering the atmospheric deterioration caused due to the seepage of toxic Pb<sup>2+</sup> ions from fly ash into local surroundings, the novel and unique applicability of the presented protocol can assist in a continuous monitoring and timely removal of Pb<sup>2+</sup> ions from fly ash, which is much required to cease its surplus transfer into the biota.

### Synthesis of acetoacetanilide-functionalized Fe<sub>3</sub>O<sub>4</sub> nanoparticles (AAA-NH<sub>2</sub>-Si@MNPs)

The synthesis of Fe<sub>3</sub>O<sub>4</sub> magnetic nanoparticles (MNPs), their subsequent silica shell coating (Si@MNPs) and further

immobilization with APTES (NH<sub>2</sub>-Si@MNPs) was performed as described in our previous study.<sup>13</sup> For the covalent functionalization of AAA with NH<sub>2</sub>-Si@MNPs, the mixture was refluxed in ethanol solution for 2 h. The resultant acetoacetanilide-functionalized Fe<sub>3</sub>O<sub>4</sub> nanoparticles (AAA-NH<sub>2</sub>-Si@MNPs) were separated magnetically, washed with ethanol and water and dried under vacuum.

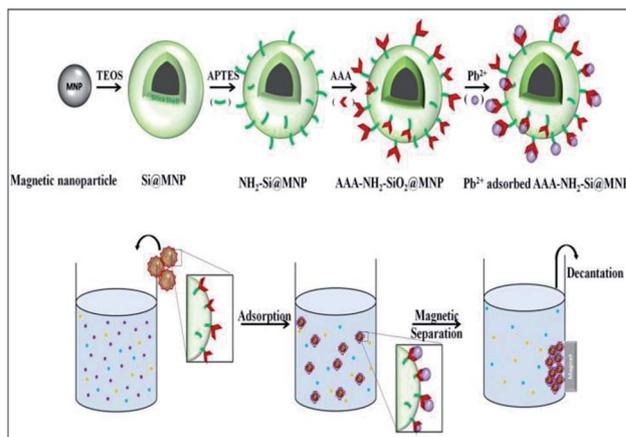
### Batch adsorption experiments

To investigate the adsorption behaviour at different pH, 0.05 g portions of AAA-NH<sub>2</sub>-Si@MNPs were suspended in 50.0 mL of sample solutions containing 25 mg L<sup>-1</sup> Pb<sup>2+</sup> at room temperature, pre-adjusted to pH values 2–6 using 0.01–0.1 M NaOH/HCl. Further, to facilitate the adsorption of metal on the functionalized surface of the nanoparticles, the suspension was sonicated for 2 min before being subjected to shaking. After reaching the adsorption equilibrium, a permanent magnet was set beside the container to move the metal-adsorbed AAA-NH<sub>2</sub>-Si@MNPs to the wall (Fig. ESI-S1†), allowing an easy decantation of the supernatant liquid (Scheme 1). The residual concentration of the metal ions in the supernatant was analysed using FAAS. The amount of Pb<sup>2+</sup> adsorbed per unit mass of adsorbents (mg g<sup>-1</sup>) was evaluated according to the following equation

$$Q = \frac{(C_0 - C_e)V}{w} \quad (1)$$

where,  $C_0$  and  $C_e$  (mg L<sup>-1</sup>) are the initial and final Pb<sup>2+</sup> concentrations in solution,  $V$  (L) is the volume of the Pb<sup>2+</sup> solution, and  $w$  (g) is the weight of dried AAA-NH<sub>2</sub>-Si@MNPs.

Adsorption capacity and isotherm experiments were carried out with 50 mL analyte solutions ranging from 50 to 400 mg L<sup>-1</sup> at different temperatures: 298, 308 and 318 K. For the adsorption kinetic equilibrium study, treatment time was varied from 5 min to 30 min. The suspension sample was taken out at different contact times, and after the separation of metal-loaded adsorbent, the residual Pb<sup>2+</sup> concentration in the clear solution was analyzed.



Scheme 1 Schematic illustration of the synthetic route of AAA-NH<sub>2</sub>-Si@MNPs followed by Pb<sup>2+</sup> removal sequence.

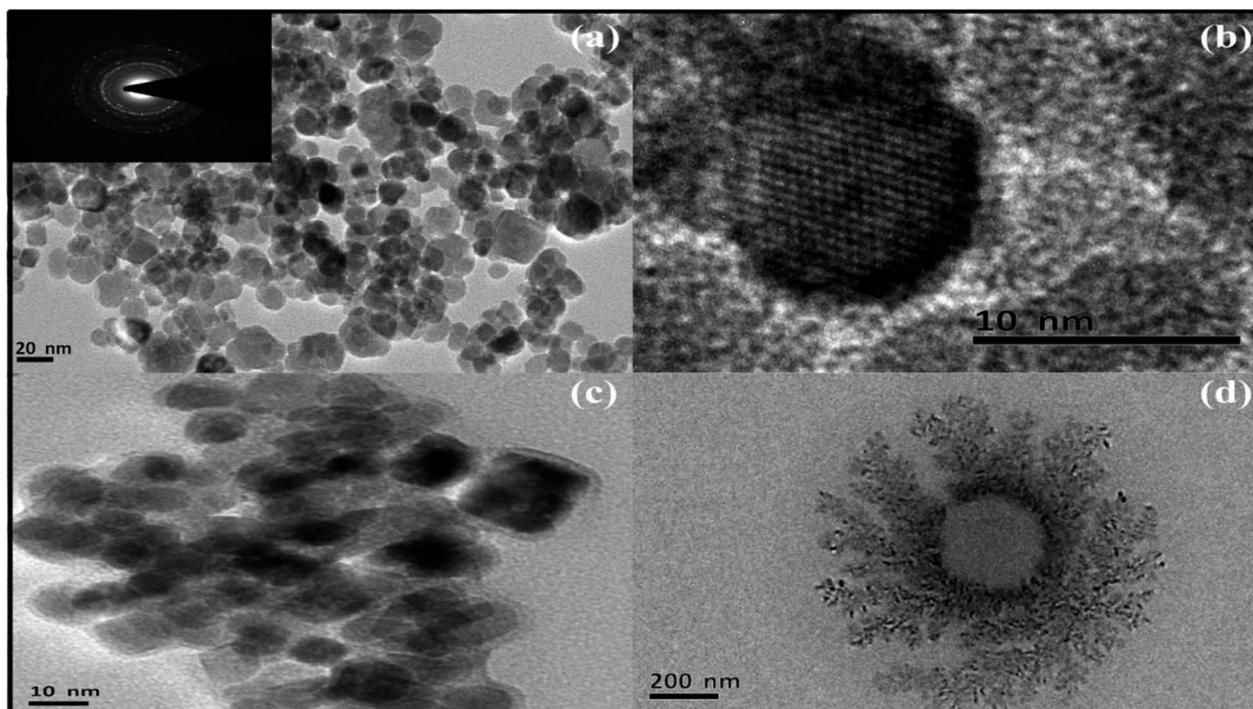


Fig. 1 TEM images of the nanoparticles obtained at different stages of synthesis (a) MNPs, (b) HR-TEM image of MNPs, (c) Si@MNPs and (d)  $\text{NH}_2$ -Si@MNPs. Inset of (a) shows SAED pattern of MNPs.

## Results and discussion

### Characterizations of AAA- $\text{NH}_2$ -Si@MNPs

**Shape, morphology and purity of nanoparticles.** The shape, size and morphological characteristics of MNPs before and after surface modifications were investigated by transmission

electron microscopy (TEM) and scanning electron microscopy (SEM). The TEM image of synthesized nanocores apparently defines the uniform structure of MNPs with an average size between 8 and 12 nm. Their crystalline nature is confirmed by the presence of an array of bright diffraction rings, which comes from the planes of magnetite in the selected area electron

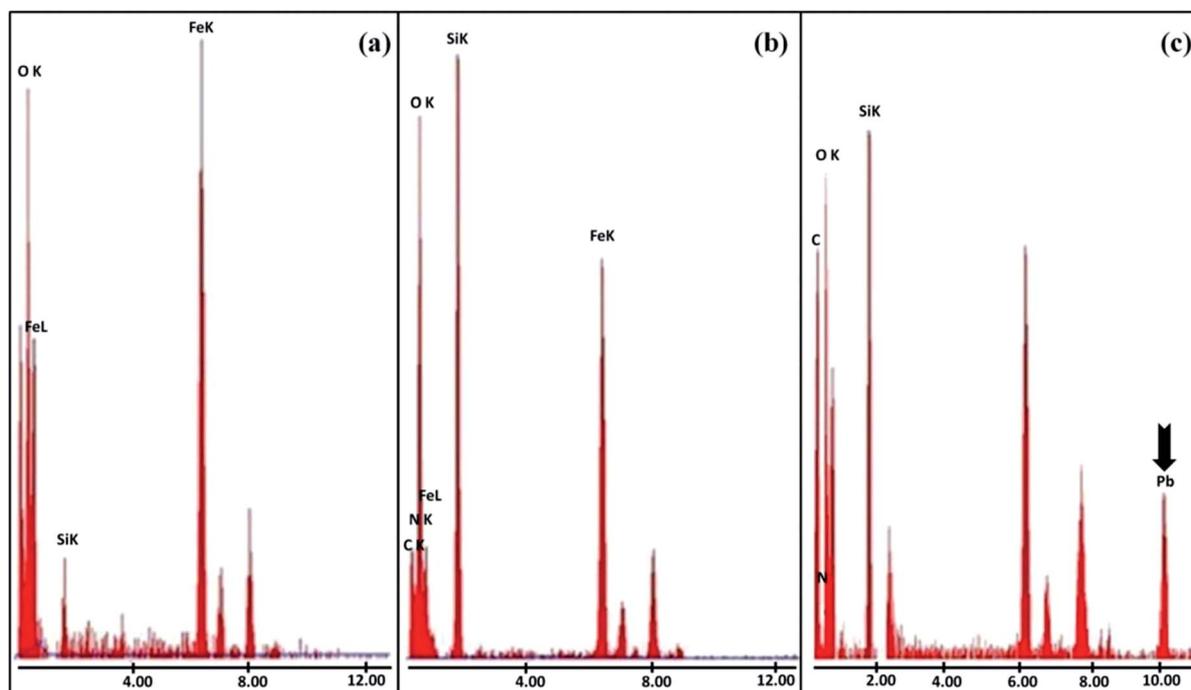


Fig. 2 EDS spectra of (a) MNPs, (b) Si@MNPs and (c)  $\text{Pb}^{2+}$ -adsorbed AAA- $\text{NH}_2$ -Si@MNPs.

diffraction (SAED) pattern (Fig. 1). In addition, the high resolution TEM (HRTEM) image shows clear 2D lattice fringes of the magnetite material. The interplanar spacing is about 0.3 nm, which corresponds well to the (2 2 0) lattice plane of the inverse spinel structure of  $\text{Fe}_3\text{O}_4$ . After the coating process, the presence of silica layers of around 3–5 nm can be easily seen at the periphery of MNPs. This core-shell feature elucidates that the  $\text{Fe}_3\text{O}_4$  nanoparticles are well embedded inside rather than simply adhering physically or blending into the silica. The deposition of organic polymer (APTES) to the surface of  $\text{Si@MNPs}$  is shown in Fig. 1d.

The SEM image captured at high magnification shows the smooth surface of the magnetic nanocore (Fig. ESI-S2<sup>†</sup>), while after encapsulation, it turns out to be rough, due to the deposition of silica coat on MNPs, which forms a uniform and continuous shell around them. In fact, the appearance of the  $\text{AAA-NH}_2\text{-Si@MNPs}$  was found to be similar to that of  $\text{Si@MNPs}$ . It implies that the silica surface efficiently retained stability and prohibited the agglomeration of the particles at the selected synthesis conditions.

**Phase and structural determination.** The surface state and phase composition of the functionalized nanoparticles were investigated by X-ray powder diffraction (XRD) (Fig. ESI-S3<sup>†</sup>). The six characteristic Bragg peaks obtained at the  $2\theta$  region of  $10\text{--}80^\circ$  indicate a highly crystalline cubic inverse spinel structure of  $\text{Fe}_3\text{O}_4$  with high phase purity. These were marked by their corresponding indices at (2 2 0), (3 1 1), (4 0 0), (4 2 2), (5 1 1) and (4 4 0) for the crystallographic faces of magnetite (JCPDS card no. 19-6290).<sup>22</sup> The average size of MNPs was estimated as approximately 12.9 nm, from full width at half-maximum (fwhm) of the (3 1 1) plane using the Debye-Scherrer relationship ( $Dhkl\ 1/4\ kl/\beta\ \cos\ \theta$ ) via line broadening in the pattern.

The diffractogram pattern of  $\text{Si@MNPs}$  significantly differs from the bare magnetic nanoparticles. A single, broad and strong diffraction hump between  $2\theta = 15\text{--}24^\circ$  confirms the presence of a poorly crystalline silica shell. Further, due to this amorphous coat, the diffraction pattern of the pure magnetite structure becomes weaker compared with that of non-shelled MNPs. As expected, after organic functionalization, there is a further decrease in the intensity with the corresponding broadening of the silica peak. It can be accredited to the lowering of scattering contrast between the walls of the silica framework and organic moiety attached over  $\text{Si@MNPs}$  and their respective synergistic effect. Besides, no noticeable reflection peak has been witnessed after the deposition of complexing active sites. This implies that organic moieties are symmetrically distributed on the surface of the functionalized nanoparticles, which can be the reason for their high adsorption efficiency. In addition, the existence of the distinguishable and persistent pattern of magnetite structure, in the latter two cases, shows crystalline phase stability.<sup>23</sup> This further signifies that the variable reaction conditions encountered during the subsequent surface modification reactions did not affect the topological structure and inherent properties of  $\text{AAA-NH}_2\text{-Si@MNPs}$ .

The EDS spectra of the isolated particles of  $\text{Si@MNPs}$  and  $\text{NH}_2\text{-Si@MNPs}$  are shown in Fig. 2. Fig. 2a illustrates that the

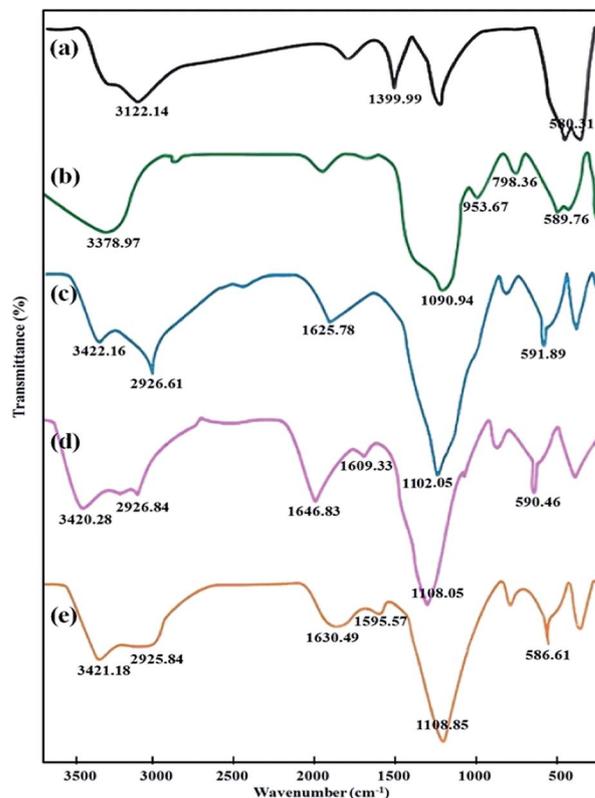


Fig. 3 FT-IR spectra of (a) MNPs, (b)  $\text{Si@MNPs}$ , (c)  $\text{NH}_2\text{-Si@MNPs}$ , (d)  $\text{AAA-NH}_2\text{-Si@MNPs}$  and (e)  $\text{Pb}^{2+}$ -adsorbed  $\text{AAA-NH}_2\text{-Si@MNPs}$ .

product comprises iron (Fe) and oxygen (O), which is due to the existence of iron oxide nanoparticles. Besides, the presence of silicon (Si) along with the other two key elements clearly reflects that rather than forming individual particles, silica is well adhered over the magnetite surface, which corroborates the findings obtained from TEM analysis. Moreover, in Fig. 2b, the appearance of a peak corresponding to N atom, along with simultaneous decrease and increase in the Fe and Si content, provide direct evidence of the incorporation of APTES over  $\text{Si@MNPs}$ .

In the FTIR spectra, an intense band around  $580\text{ cm}^{-1}$  is assigned to the typical Fe–O vibrations of the magnetite structure (Fig. 3). The pronounced changes upon silica encapsulation can be identified by the appearance of Si–O–Si symmetric, Si–O symmetric and Si–O–Si asymmetric stretching modes observed at 798, 953 and  $1090\text{ cm}^{-1}$ , respectively, which are the characteristic absorption bands of amorphous siliceous matrix.<sup>24</sup> In fact, Fe–O adsorption vibration in the same vicinity is decreased to lower intensity, which further verifies the surface coating of MNPs. Compared to  $\text{Si@MNPs}$ , in  $\text{NH}_2\text{-Si@MNPs}$ , the distinguishable peak of Si–OH stretch has been turned into a very weak shoulder, signifying that the surface silanol groups are being substituted by aminosilane groups. Though N–H vibration bands are not visible due to the superposition of those with those of water at 1625 and in the  $3300\text{--}3500\text{ cm}^{-1}$  range, C–H stretch due to aminopropyl moieties is well noticed as an edge at  $2926\text{ cm}^{-1}$ . In addition, the immobilization of ligand ( $\text{AAA-NH}_2\text{-Si@MNPs}$ ) can be seen from the peak around

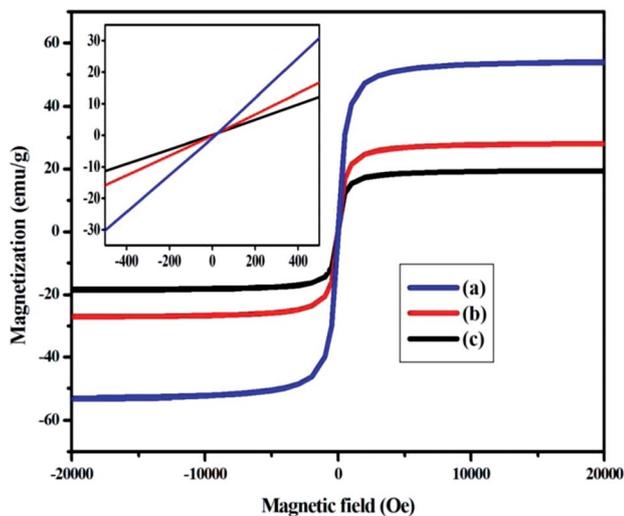


Fig. 4 Magnetic hysteresis loops of (a) MNPs, (b) Si@MNPs, (c) AAA-NH<sub>2</sub>-Si@MNPs at room temperature. Inset shows enlargement of graph near origin.

1609 cm<sup>-1</sup> due to the C=N stretching vibration mode, suggesting the formation of covalent linkage *via* amine functionality.<sup>15</sup> Upon metal complexation, a noticeable shift of C=N and C=O frequencies to lower wavenumbers in conjunction with their decreased intensities elucidates the active role of these sites in the chemical adsorption of Pb<sup>2+</sup> ions.

**Property characterization.** Fig. 4 shows the saturation magnetization responses of the MNP, Si@MNP, and AAA-NH<sub>2</sub>-Si@MNP powders upon application of various external magnetic fluxes from -20 000 to 20 000 Oe at room temperature. The superparamagnetic behaviour can be easily predicted from the inset, as the obtained plots show negligible coercivity and remanence in the absence of external magnetic field with both magnetization and demagnetization curves passing through the origin. Furthermore, the saturation magnetization ( $M_s$ ) of magnetite nanoparticles (53 emu g<sup>-1</sup>) is smaller than that of bulk magnetite (92 emu g<sup>-1</sup>).<sup>25</sup>

This decrease elucidates the precise role of particle size, which is proportional to the extent of magnetization of a particle in an external applied field. Hence, a smaller saturation magnetization value for the magnetic particles of nano range compared to bulk material is reasonable.

After stabilization of MNPs with silica (Si@MNPs) followed by the covalent immobilization of the functional moieties (AAA-NH<sub>2</sub>-Si@MNPs),  $M_s$  values are reduced to 28 emu g<sup>-1</sup> and 19 emu g<sup>-1</sup>, respectively. This is undoubtedly related to the increase in the surface disorder of MNPs *via* the contribution of the non-magnetic silica shell and the incorporated complexing groups to the total mass of the nanoparticles.<sup>26</sup>

**Effect of pH on lead adsorption and mechanism discussion.** pH of the aqueous phase is an important parameter to be considered, as it can strongly affect the surface charge of the adsorbent. Besides, Pb<sup>2+</sup> ions exist as different proportions of Pb<sup>2+</sup>, Pb(OH)<sup>+</sup>, Pb(OH)<sub>2</sub><sup>0</sup> and Pb(OH)<sub>3</sub><sup>-</sup> at different pH values. In this study, the adsorption behaviour was investigated in the pH range of 2 to 6 as metal species predominantly remain as

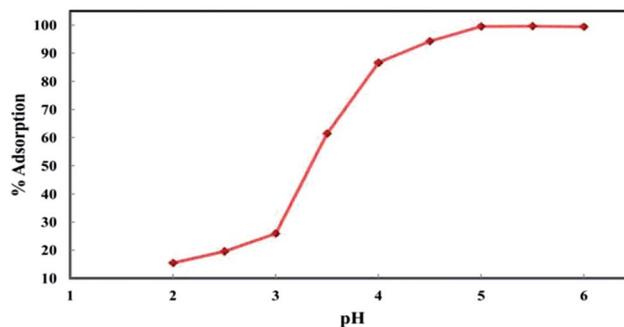


Fig. 5 Effect of pH on the adsorption behaviour of AAA-NH<sub>2</sub>-Si@MNPs for Pb<sup>2+</sup> ions (conditions: initial Pb<sup>2+</sup> concentration: 50 mg L<sup>-1</sup>, pH: 5.0, adsorbent dose: 1 g L<sup>-1</sup>, contact time: 30 min, reaction temperature: 298 K).

divalent free ions in solution at pH < 6.<sup>9,27</sup> The curve representing the percentage adsorption as a function of initial pH is illustrated in Fig. 5.

As can be seen, AAA-NH<sub>2</sub>-Si@MNPs show diminished affinity for metal adsorption at low pH values. This could be attributed to three factors. First, in an acidic pH range, the surface functional groups are protonated to various degrees. By this, the availability of active binding sites for the metal uptake is reduced to a greater extent. Second, due to the coulombic repulsion between the positively charged surface and metal species bearing the same charge, the approach of metal ions to the nanoadsorbent is significantly hindered. Third, a high concentration of protons leads to a keen competition between analytes and hydrogen ions for the same binding sites.<sup>17,28</sup> Nevertheless, with the rise in pH value, the adsorption of Pb<sup>2+</sup> ions increases sharply and reaches a plateau at pH 5. Similar trends are observed in zeta potential measurements at different pH values (Fig. ESI-S4†). They showed that the surface of the functionalized nanoparticles becomes negatively charged beyond the point of zero charge ( $P_{ZC}$ ), which is around 3.9. This not only increases the density of active functional groups by deprotonation, but also enhances their availability to metal cations by preventing aggregation. Hence, all the succeeding investigations were performed at initial pH 5.

The presence of metal in the adsorbent framework is witnessed by the existence of a distinguishable and well-resolved peak of Pb in the EDS spectrum (Fig. 2c), which gave a pivotal evidence of metal adsorption at the desired pH.

To determine the coordination sites that may be involved in complexation, the FTIR spectra of the functionalized nanoparticles before and after metal adsorption (Fig. 3d and e) were compared. As can be seen, AAA-NH<sub>2</sub>-Si@MNPs showed noticeable changes after binding to the Pb<sup>2+</sup> ions. They exhibited the band of C=N in the region 1593–1597 cm<sup>-1</sup>, showing a bathochromic shift, which ensures the participation of nitrogen of the azomethine group in metal ion coordination. Moreover, the C=O band at 1646 cm<sup>-1</sup> for the amide carbonyl group was shifted by 10–13 cm<sup>-1</sup> to a lower wavenumber, which signifies that the amide carbonyl oxygen is bonded to the Pb<sup>2+</sup> ions. In fact, the intensities of the peaks are also weakened, which prove the active involvement of these sites for metal adsorption.

**Table 1** Kinetic parameters and correlation coefficients for adsorption of  $\text{Pb}^{2+}$  on AAA- $\text{NH}_2$ -Si@MNPs. (Conditions: initial  $\text{Pb}^{2+}$  concentration: 50  $\text{mg L}^{-1}$ , pH: 5.0, adsorbent dose: 1  $\text{g L}^{-1}$ , reaction temperature: 298 K)

Pseudo-first-order model $\ln(q_e - q_t) = \ln q_e - k_1 t$			Pseudo-second-order model $\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}$		
$q_e(q_{\text{exp}})^a$ ( $\text{mg g}^{-1}$ )	$k_1$ ( $\text{min}^{-1}$ )	$R^2$	$q_e(q_{\text{exp}})^a$ ( $\text{mg g}^{-1}$ )	$k_2$ ( $\times 10^{-5} \text{ g mg}^{-1} \text{ min}^{-1}$ )	$R^2$
286.4(380.1)	0.2016	0.6973	380.2(380.1)	1.39	0.9766

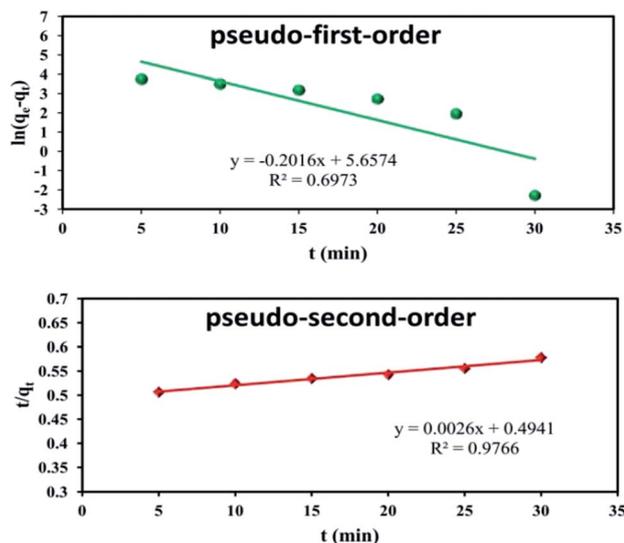
<sup>a</sup> Experimental adsorption capacity value.

Similar results have been observed in previous reports of nanoadsorbents carrying these functional groups.<sup>29–31</sup> Hence, it is reasonable that amide carbonyl and imine functional groups possess strong chelating ability for  $\text{Pb}^{2+}$  ions. It further implies that the covalent immobilization of acetacetanilide over the surface of  $\text{NH}_2$ -Si@MNPs strongly contributes to the efficient capturing of  $\text{Pb}^{2+}$  in aqueous solution.

**Adsorption kinetics.** The effect of adsorption kinetics is an essential parameter to be studied as the removal rate directly affects the operation cost. It was found that heavy metal ion uptake was very fast, and the process almost completely reached equilibrium within 30 min, which is much shorter than what has been previously reported.<sup>14,16</sup> The high adsorption rate can be attributed to the presence of sufficient adsorption sites and ease of their accessibility as well as strong complexation ability towards  $\text{Pb}^{2+}$  ions. To check the suitable kinetic model with corresponding model parameters, the obtained data were formulated to the linearized form of pseudo-first- and second-order models.

$$\ln(q_e - q_t) = \ln q_e - k_1 t \quad (2)$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e} \quad (3)$$



**Fig. 6** Linearized pseudo- (a) first-order and (b) second-order kinetic plots for the adsorption of  $\text{Pb}^{2+}$  on AAA- $\text{NH}_2$ -Si@MNPs.

The values of the obtained kinetic parameters are summarized in Table 1, and plots are depicted in Fig. 6. As can be seen, the experimental value ( $q_{\text{exp}}$ ) for pseudo-second-order kinetic model is in good agreement with the calculated value ( $q_e$ ). Besides, the high  $R^2$  value shows the applicability of this model to describe the kinetic profile of the present system. Hence, it can be speculated that the adsorption rate is dependent only on the sorption capacity, but not the adsorbate concentration, while the sorption efficiency is directly linked to the number of active sites occupied on the adsorbent. It further indicates that the adsorption of  $\text{Pb}^{2+}$  ions onto AAA- $\text{NH}_2$ -Si@MNPs is based on the chemisorption controlled rate of the process, involving the valence forces through the sharing or exchange of electrons between metal ion and adsorbent.<sup>32</sup> Consequently, it is implied that the nature of interaction between adsorbent and  $\text{Pb}^{2+}$  ions is chemical, involving metal complexation as a dominant mechanism, which correlates well with the results obtained from FTIR studies.<sup>16</sup>

**Adsorption isotherms.** Understanding the interaction behaviour between the analyte and the adsorbent is of fundamental importance and can be envisaged by employing different adsorption isotherms at pre-optimized conditions. In the present study, Langmuir and Freundlich adsorption isotherm models were used. The Freundlich model assumes multilayer, reversible and non-ideal adsorption at the active sites with exponential distribution of energies, which endorses the heterogeneity of the surface. Unlike the Freundlich isotherm, the Langmuir isotherm is based on the monolayer and homogenized coverage of the adsorbent surface, where all sorption sites are identical and energetically equivalent. The experimental equilibrium data at different temperatures were evaluated according to the linear equations of these models given below,<sup>15</sup> and the curve fitting results are compiled in Table 2 (Fig. ESI-S5 and S6†).

$$\frac{C_e}{q_e} = \frac{1}{q_m K_L} + \frac{C_e}{q_m} \quad (4)$$

$$\ln q_e = \frac{\ln C_e}{n} + \ln K_F \quad (5)$$

where  $C_e$  and  $q_e$  are the concentration and adsorption capacity at equilibrium, and  $q_m$  and  $K_L$  are Langmuir constants, representing the maximum adsorption capacity and energy of adsorption ( $\text{L mg}^{-1}$ ), respectively.  $K_F$  and  $n$  are Freundlich constants related to adsorption capacity and intensity, respectively. Comparing the correlation coefficients, the Langmuir

**Table 2** Langmuir and Freundlich isotherm constants, equilibrium parameters and correlation coefficients for adsorption of  $\text{Pb}^{2+}$  on AAA- $\text{NH}_2$ -Si@MNPs (conditions: initial  $\text{Pb}^{2+}$  concentration: 50 to 400  $\text{mg L}^{-1}$ , pH: 5.0, adsorbent dose: 1  $\text{g L}^{-1}$ , contact time: 30 min, reaction temperature: 298 K, 308 K and 318 K)

Isotherm model	Estimated isotherm parameters	Temperature		
		298 K	308 K	318 K
Langmuir $\frac{C_e}{q_e} = \frac{1}{q_m K_L} + \frac{C_e}{q_m}$	$R^2$	0.9905	0.9735	0.9709
	$q_m(q_{\text{exp}})^a$	380.2(380.1)	389.1(386.1)	392.2 (392.4)
	$K_L$	0.822	0.988	1.214
Freundlich $\ln q_e = \frac{\ln C_e}{n} + \ln K_F$	$R^2$	0.8595	0.9528	0.8122
	$K_F$	147.6	188.3	184.9
	$n$	2.88	4.41	3.36

<sup>a</sup> Experimental adsorption capacity value.

**Table 3** Estimated values of thermodynamic parameters at different temperatures

Temperature	$\Delta G$ ( $\text{kJ mol}^{-1}$ )	$\Delta H$ ( $\text{kJ mol}^{-1}$ )	$\Delta S$ ( $\text{J mol}^{-1}\text{K}^{-1}$ )
298 K	-29.84	15.36	151.65
308 K	-31.32		
318 K	-32.88		

model yields a more accurate fit to the experimental data than the Freundlich model. Further, it shows a clear consistency between the calculated ( $q_m$ ) and experimental values ( $q_{\text{exp}}$ ) of the adsorption capacity at equilibrium. Therefore, it can be considered that monolayer adsorption takes place at specific sites present on the surface of AAA- $\text{NH}_2$ -Si@MNPs, which are energetically identical. It further confirms that chemisorption occurs due to the complexation between  $\text{Pb}^{2+}$  ions and the organic groups present on the surface of the nano-adsorbent.<sup>6,7</sup>

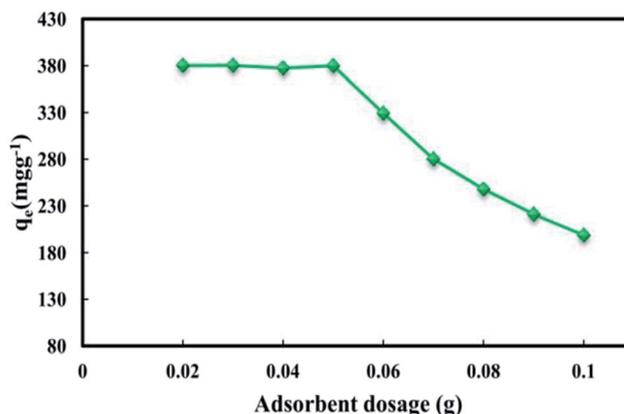
### Adsorption thermodynamics

The improved sorption performance of AAA- $\text{NH}_2$ -Si@MNPs with elevated temperature elucidates that the adsorption process is thermodynamically driven. Thermodynamic parameters quantified with the measured data under a preset range of temperatures are listed in Table 3. Fig. ESI-S7† shows the plot of  $\ln K_L$  versus  $1/T$  fitted to a straight line. The positive enthalpy change found for the system reflects the endothermic nature of the process. This phenomenon is usually observed in the adsorption systems based on site-specific interactions caused by the formation of chemical bonds between the surface of adsorbent and the heavy metal ions. Hence, the adsorption process can be considered as chemisorption, because had it been only physisorption, the enthalpy of the system should have been exothermic. The positive  $\Delta S$  value indicates an increase in the disorder of the system, which comes from the release of water molecules surrounding the hydrated metal ions and solid-solution interface to the bulk aqueous medium during the metal complexation process. Thereby, it results in preferential affinity of  $\text{Pb}^{2+}$  ions towards the adsorbent surface. The negative sign of  $\Delta G$  implies spontaneity of the reaction, which comes

from the difference between energetic potentials of the system components. It indicates that the binding energy of the metal-adsorbent is stronger than the metal-aqueous phase, which is considered to be the driving force of the redistribution of  $\text{Pb}^{2+}$  ions in the system and their rapid sorption onto AAA- $\text{NH}_2$ -Si@MNPs. The increase in negative magnitude of this parameter with the rise in experimental temperature demonstrates that adsorption is more favourable at higher temperatures, which eventually leads to an increase in the adsorption efficiency. The acquired results are in agreement with those of previous studies on the adsorption of  $\text{Pb}^{2+}$  ions.<sup>16,17</sup>

**Effect of the adsorbent dosage.** The optimal amount of adsorbent greatly influences the process cost by minimizing waste and maximizing the quantitative recovery of heavy metal ions. Therefore, the optimal adsorbent dosage in terms of the adsorption capacity of the functionalized nanoparticles was investigated at pH 6.0, by varying the adsorbent amount from 0.01 to 0.1 g.

Fig. 7 illustrates that 0.05 g of AAA- $\text{NH}_2$ -Si@MNPs is very effective for the adsorption of  $\text{Pb}^{2+}$  ions. Beyond this, the adsorption capacity remarkably decreases. The observed trend can be explained on the basis of availability of binding sites,



**Fig. 7** Effect of adsorbent dosage on the adsorption capacity of  $\text{Pb}^{2+}$  ions (conditions: initial  $\text{Pb}^{2+}$  concentration: 50  $\text{mg L}^{-1}$ , pH: 5.0, adsorbent dose: 1  $\text{g L}^{-1}$ , contact time: 30 min, reaction temperature: 298).

which rises with the increase in adsorbent dosage. However, the concentration of  $\text{Pb}^{2+}$  in the aqueous solution is fixed, and once nearly all the ions are adsorbed by the adsorbent, the number of vacant active sites grows, which would no longer participate in the adsorption process.<sup>17</sup> This ultimately leads to a decrease in the adsorption capacity.

**Desorption *via* ultrasonication and stability.** To broaden the economic dimensions and practical significance of a nano-adsorbent for environmental purposes, its regeneration is highly desirable. Moreover, it aids in the effective separation and recovery of heavy metals for their reutilization or safe disposal.

As can be seen earlier (Fig. 5), the functionalized nanoparticles show diminished affinity towards the target analyte at low pH. Hence, it is an indication that the adsorbent could be generated simply in an acidic environment. Therefore, several acids and their binary mixtures with different concentrations were evaluated to find the suitable eluent for simultaneous regeneration of the nanoadsorbent and recovery of the analyte. However, highly concentrated acids and their prolonged contact with the AAA-NH<sub>2</sub>-Si@MNPs can engulf the active species present on its surface and reduce its life span. Considering this verity, ultrasonic-assisted mild acidic treatments were used to reduce the extent of structural damage and to increase the lifetime of nanoadsorbent for multiple usage.

A contact time of 5 min was used as the preset standard. It can be seen (Table ESI-S1†) that  $\text{Pb}^{2+}$  desorption is highly favoured with HNO<sub>3</sub> in comparison to other desorptive reagents. Further, metal recovery seems to be compromised when nitric acid concentration and volume are less than 0.1 M and 4 mL, respectively. The effective desorption of  $\text{Pb}^{2+}$  ions by HNO<sub>3</sub> has also been reported in earlier studies<sup>20,33,34</sup> that support our findings. To ensure acidic resistance, the magnetic nano-adsorbent was suspended in 4 mL portions of 0.1 M nitric acid. The concentration of Fe, which was measured after a 72 h contact time, showed negligible etching (<0.1 ppm). This shows that Fe is strongly retained within the silica core, and the functionalized nanoparticles are highly stable towards encountered conditions. Thus, employed elution parameters are found to be optimal to concentrate and recover  $\text{Pb}^{2+}$  ions without impairing the stability of AAA-NH<sub>2</sub>-Si@MNPs.

**Effect of interfering ions.** The prime source of competitive adsorption is the presence of different metal ions and electrolytes, which cause persistent hindrance to the binding affinity of analyte for the active sites and strongly inhibit the performance of the functionalized nanoparticles. Moreover, the non-selective nature of adsorbents limits the reusability of heavy metal ions.<sup>7</sup> Recently, different materials have been reported for the efficient adsorption of  $\text{Pb}^{2+}$  ions, but they apparently lose their utility in real environmental applications as no attention has been paid to determine their selectivity behaviour in the presence of other metals.<sup>1,8,33</sup> Thus, in the present study, the relevance of nano-adsorbent for the selective separation of  $\text{Pb}^{2+}$  ions from complicated matrices was assessed by treating binary sample solutions containing 0.5 mg L<sup>-1</sup> of  $\text{Pb}^{2+}$  ions and varying the concentration of interfering ions with the pre-optimized experimental procedure. The analytical data, representing the

maximum tolerable concentration of the investigated ions causing a relative error of not more than 5% in the recovery of the target analyte, is as follows: 3.0 g L<sup>-1</sup> K<sup>+</sup> and Na<sup>+</sup>, 2.0 g L<sup>-1</sup> Ca<sup>2+</sup> and Mg<sup>2+</sup>, 0.02 g L<sup>-1</sup> Cd<sup>2+</sup>, 0.04 g L<sup>-1</sup> Cu<sup>2+</sup>, Ni<sup>2+</sup> and Co<sup>2+</sup>, 0.05 g L<sup>-1</sup> Zn<sup>2+</sup>, 0.8 g L<sup>-1</sup> Cr<sup>3+</sup> and Fe<sup>3+</sup>, 1.0 g L<sup>-1</sup> Al<sup>3+</sup>, 2.0 g L<sup>-1</sup> Cl<sup>-</sup>, 5.0 g L<sup>-1</sup> NO<sub>3</sub><sup>2-</sup> and CH<sub>3</sub>COO<sup>-</sup> and 6.0 g L<sup>-1</sup> SO<sub>4</sub><sup>2-</sup>. It is evident from the results that AAA-NH<sub>2</sub>-Si@MNPs possess a high capacity for tolerance of the various interfering cations and anions, which are inevitably associated with  $\text{Pb}^{2+}$  at trace levels.

This specificity and high affinity towards the target analyte can be explained on the basis of anchored organic functionalities over the surface of the functionalized nanoparticles. As mentioned earlier, amide carbonyl and imine functional groups possess a strong chelating ability for the analyte. This in turn leads to the selective adsorption of  $\text{Pb}^{2+}$  ions due to the formation of stable metal complexes. In fact, the tendency of the preferential uptake of  $\text{Pb}^{2+}$  on different adsorbents containing imine and carbonyl functional groups has already been reported in other studies.<sup>29-31</sup>

Besides functional groups, the other physiochemical properties of the metal ion can strongly influence the extent to which it binds to the material. Considering the concept of hydration enthalpy, which is the energy released when H<sub>2</sub>O molecules in the solution attach themselves to the available metal ions.

The heavy metal that possesses the lowest hydration energy can be transformed into bare ions most easily due to its ease of separation from the associated water molecules. It has the following sequence for the studied heavy metal ions: Al<sup>3+</sup> > Cr<sup>3+</sup> > Fe<sup>3+</sup> > Ni<sup>2+</sup> > Cu<sup>2+</sup> > Co<sup>2+</sup> > Zn<sup>2+</sup> > Cd<sup>2+</sup> >  $\text{Pb}^{2+}$ . As can be seen,  $\text{Pb}^{2+}$  has a lowest hydration enthalpy in comparison to that of other ions, which facilitates its easy availability to the existing functional groups on the surface of AAA-NH<sub>2</sub>-Si@MNPs.<sup>35,36</sup> Thus, it can be efficiently and quickly captured by the nanoadsorbent even in a competitive metal environment. Likewise, both the high electronegativity and ionic radius of  $\text{Pb}^{2+}$  in contrast to other ions can aid constructively for its selective adsorption (Table ESI-S2†).<sup>37</sup>

Apart from these factors, earlier, Inoue *et al.* pointed out that the type of supporting material may significantly affect the selectivity behaviour of an adsorbent.<sup>38</sup> Further, it was

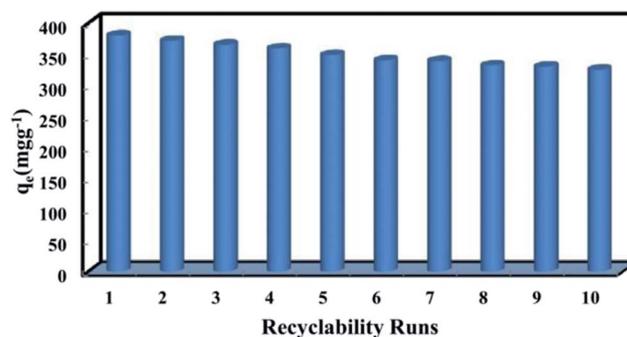


Fig. 8 The adsorption performance of AAA-NH<sub>2</sub>-Si@MNPs by multiple regeneration cycles (conditions: initial  $\text{Pb}^{2+}$  concentration: 50 mg L<sup>-1</sup>, pH: 5.0, adsorbent dose: 1 g L<sup>-1</sup>, contact time: 30 min, desorption time: 5 min reaction temperature: 298 K).

**Table 4** Analysis of Pb<sup>2+</sup> ions in different real samples (conditions: pH: 5.0, adsorbent dose: 1 g L<sup>-1</sup>, contact time: 30 min, desorption time: 5 min, reaction temperature: 298 K)

Sample	Added <sup>c</sup> (μg L <sup>-1</sup> or μg g <sup>-1</sup> )	Found (μg L <sup>-1</sup> or μg g <sup>-1</sup> )	Recovery (%)
Yamuna river water	—	0.29 ± 0.01 <sup>e</sup>	—
Rain water	10.0	10.11 ± 0.16	98.3
FA1 <sup>a</sup>	—	5.72 ± 0.14	—
	10.0	15.76 ± 0.05	100.3
FA2 <sup>a</sup>	—	47.33 ± 0.58	—
	10.0	57.26 ± 0.80	99.9
FA3 <sup>a</sup>	—	46.76 ± 0.85	—
	10.0	56.02 ± 0.89	98.7
FA4 <sup>a</sup>	—	48.07 ± 1.18	—
	10.0	57.58 ± 1.12	99.2
FA1 <sup>b</sup>	—	47.94 ± 0.52	—
	10.0	57.10 ± 1.43	98.6
FA2 <sup>b</sup>	—	39.15 ± 0.50	—
	10.0	49.25 ± 0.88	100.2
FA3 <sup>b</sup>	—	41.84 ± 0.27	—
	10.0	51.26 ± 1.19	98.9
FA4 <sup>b</sup>	—	41.40 ± 0.52	—
	10.0	50.66 ± 0.99	98.6
	—	40.86 ± 0.90	—
	10.0	50.34 ± 0.80	99.0

<sup>a</sup> Mycorrhizal-treated fly ash samples from Thermal Power Plant.

<sup>b</sup> Mycorrhizal-treated fly ash samples from Fertilizer Plant. <sup>c</sup> For water samples. <sup>d</sup> For fly ash samples. <sup>e</sup> Mean of five determinations ±ts/√n (t<sub>4,0.05</sub> = 2.78).

emphasized that the matrix may cause the active sites to orient in a manner to capture a particular metal ion having entirely unique physiochemical properties.<sup>39</sup> Indeed, the obtained results clearly demonstrate that the substrate material is positioning the active sites specifically enough to particularly occupy Pb<sup>2+</sup> ions and result in the formation of a strong and stable metal chelate. Besides all these, the significance of experimental conditions to determine the selectivity cannot be subsided.<sup>40</sup> Hence, it can be inferred that the specificity of an adsorbent towards a particular metal is collectively dependent on all of the above-mentioned parameters. In addition, due to the high tolerance of various interfering ions, the method can be successfully implemented to remove Pb<sup>2+</sup> ions from environmental samples.

**Reusability.** Besides an economic necessity, reusability of an adsorbent is an essential pathway to achieve the goal of sustainability, as it facilitates the continuous separation of heavy metals for their further recycling. But in some studies, not much emphasis has been given to the reutilization of adsorbents,<sup>1,35,36</sup> which limits their application in practical considerations. Therefore, in order to fulfil this purpose, ten successive adsorption–desorption runs using the same adsorbent were performed. Excellent recyclability and mechanical strength can be easily recognized by viewing the consistency in the performance of AAA-NH<sub>2</sub>-Si@MNPs, in terms of adsorption capacity during each regeneration cycle (Fig. 8). Besides, the morphology and structure remain intact even after repetitive usage, and there is no sign of obvious agglomeration, which is demonstrated by the TEM and SEM images of the recovered functionalized nanoparticles (Fig. ESI-S8†). Likewise, the saturation magnetization curve shows that the decrease in M<sub>s</sub> value is very less than that of fresh AAA-NH<sub>2</sub>-Si@MNPs (Fig. ESI-S9†). This substantiates their good structural stability, which is not affected by the repeated stirring and acidic treatment throughout the cyclic process.

However, a perpetual but minor decline in the adsorption capacity values of AAA-NH<sub>2</sub>-Si@MNPs is observed during the ten cycles. It can be due to the partial loss of some of the active sites to which Pb<sup>2+</sup> ions are irreversibly bound, leading to their unavailability for further adsorption. But even then, it retains more than 85% of its original capacity in the final cycle. In fact, the presence of the magnetic core makes the separation process very easy and greatly reduces the loss of adsorbent with repetitive usage. Thus, excellent reusability in conjunction with the high structural stability and efficiency of the nanoadsorbent for the removal of Pb<sup>2+</sup> ions makes it a potential candidate to combat ecological distress.

**Application to real samples.** The applicability of AAA-NH<sub>2</sub>-Si@MNPs was tested in rain water, river water and mycorrhizal-treated fly ash samples. These environmental samples contain different miscellaneous ions, which might compete for the interaction with the nanoadsorbent. Consequently, validation was done by spiking a known amount of Pb<sup>2+</sup> in the procured samples. The analytical results along with the recoveries for the spiked samples are presented in Table 4. Quantitative enrichment of trace levels of Pb<sup>2+</sup> and excellent agreement between

**Table 5** Various solid phase extraction systems for Pb<sup>2+</sup> ions determination and their analytical characteristics

Analytical technique	Adsorption capacity (mg g <sup>-1</sup> )	Reusability (cycle)	Equilibration/ Elution time (min)	Ref.
Fe <sub>3</sub> O <sub>4</sub> -TETA-CMCS-FAAS	370.63	5	90/300	6
Ion-imprinted crown ether-AAS	27.95	5	60/120	7
Titanate/Fe <sub>3</sub> O <sub>4</sub> -ICPS	382.3	2	60/—	9
Fe <sub>3</sub> O <sub>4</sub> @SiO <sub>2</sub> -NH <sub>2</sub> -ICP-AAS	243.9	5	480/20	16
EDTA modified chitosan/SiO <sub>2</sub> /Fe <sub>3</sub> O <sub>4</sub> -MP-AES	123.5	12	720/600	17
Fe <sub>3</sub> O <sub>4</sub> @SiO <sub>2</sub> @1,3-CalixCrown-ICP-AES	—	3	120/—	20
P(A-O)/AT nano-adsorbent-AAS	109.9	—	120/—	31
Fe <sub>3</sub> O <sub>4</sub> /cyclodextrin-ICP-MS	64.5	4	45/180	34
AAA-NH <sub>2</sub> -Si@MNPs-FAAS	380.2	10	30/5	Present

the preconcentrated and spiked values undoubtedly demonstrates the sensitivity, specificity and versatility of AAA-NH<sub>2</sub>-Si@MNPs for extensive ecological applications.

**Comparative analysis.** To reinforce the utility of AAA-NH<sub>2</sub>-Si@MNPs, its important analytical features have been compared with some recent literature citations and are listed in Table 5. As can be seen, the functionalized nanoparticles have a very high loading capacity for the preconcentration of Pb<sup>2+</sup> ions. Although titanate/Fe<sub>3</sub>O<sub>4</sub> nanocomposites<sup>9</sup> display a slightly enhanced quantitative binding capacity, the material we fabricate presents a better capacity to be recycled, very less desorption time, faster kinetics and higher specificity over other preconcentrating matrices. Also, the good reusability of EDTA-modified chitosan/SiO<sub>2</sub>/Fe<sub>3</sub>O<sub>4</sub> adsorbent<sup>17</sup> is superseded by the high adsorption capacity and low adsorption equilibrium time of the synthesized AAA-NH<sub>2</sub>-Si@MNPs. In addition, when judged against non-magnetic nanomaterials, the developed system possesses rapid and convenient operation and separation, and economic dominance due to the existence of superparamagnetic inexpensive core material. In fact, the adsorbent is more compliant for practical purposes, due to the non-fragile nature of silica-protected MNPs, which enhances their durability and reusability in comparison to adsorbents where surface modifications are done on the bare iron oxide.<sup>6,9,34</sup>

## Conclusions

The stepwise modification of iron oxide nanoparticles was performed to obtain a novel and effective magnetically-driven multifunctional solid-phase nano-adsorbent, which exhibited excellent performance for lead removal. A superparamagnetic core provided ease of separation, while silica shell encapsulation endowed superior dispersibility and stability to the nanoparticles, by preventing their aggregation and chemical decomposition. Exclusive selectivity towards the target analyte is due to the collective contribution of various factors, including anchored functional groups, substrate material, experimental conditions and physicochemical properties of the analyte. The assistance of sonication with mild acidic treatment in the elution process offers a rapid recovery of Pb<sup>2+</sup> ions without damaging the structure of the functionalized nanoparticles. Cost effectiveness of embedded MNPs, good material stability, high adsorption capacity, ease of fabrication, and superior reusability over multiple adsorption/desorption cycles are some other valuable properties of AAA-NH<sub>2</sub>-Si@MNPs. Thus, by the constructive integration of efficiency, selectivity and reusability, this finding paves a sustainable pathway for the systematic recovery and recycling of Pb<sup>2+</sup> ions. Besides, the novel and unique applicability in mycorrhizal-treated fly ash samples can be envisioned as a powerful source to lower the leachable metal content to such an extent that the ecological stress is balanced.

## Acknowledgements

Aditi Puri expresses her gratitude to the University Grant Commission, Delhi, India for the award of Senior Research

Fellowship. Also, due thanks to USIC-CLF, DU for HR-XRD, HR-TEM and VSM analysis.

## Notes and references

- 1 Y. L. F. Musico, C. M. Santos, M. L. P. Dalida and D. F. Rodrigues, *J. Mater. Chem. A*, 2013, **1**, 3789–3796.
- 2 T. E. Norgate and W. J. Rankin, The role of metals in sustainable development, in *Proceedings of green processing*, Cairns, 2002, pp. 49–55.
- 3 J. R. Dodson, A. J. Hunt, H. L. Parker, Y. Yang and J. H. Clark, *Chem. Eng. Process.*, 2012, **51**, 69–78.
- 4 WHO, Exposure to lead: A major public health concern, *Department of Public Health and Environment*, World Health Organization, Geneva, 2010. <http://www.who.int/ipcs/features/lead.pdf>.
- 5 WHO, Lead exposure, in *Comparative quantification of health risks*, World Health Organization, Geneva, 2004, pp. 1495–1542, <http://www.who.int/publications/cra/chapters/volume2/1495-1542.pdf>.
- 6 S. P. Kuang, Z. Z. Wang, J. Liu and Z. C. Wu, *J. Hazard. Mater.*, 2013, **260**, 210–219.
- 7 X. Luo, L. Liu, F. Deng and S. Luo, *J. Mater. Chem. A*, 2013, **1**, 8280–8286.
- 8 Z. Ma, D. Zhao, Y. Chang, S. Xing, Y. Wu and Y. Gao, *Dalton Trans.*, 2013, **42**, 14261–14267.
- 9 F. Liu, Y. Jin, H. Liao, L. Cai, M. Tong and Y. Hou, *J. Mater. Chem. A*, 2013, **1**, 805–813.
- 10 S. S. Bayazit and I. Inci, *J. Ind. Eng. Chem.*, 2013, **19**, 2064–2071.
- 11 R. Sitko, E. Turek, B. Zawisza, E. Malicka, E. Talik, J. Heimann, A. Gagor, B. Feista and R. Wrzalik, *Dalton Trans.*, 2013, **42**, 5682–5689.
- 12 B. Wang, H. Wu, L. Yu, R. Xu, T.-T. Lim and X. W. (David) Lou, *Adv. Mater.*, 2012, **24**, 1111–1116.
- 13 R. K. Sharma, Y. Monga, A. Puri and G. Gaba, *Green Chem.*, 2013, **15**, 2800–2809.
- 14 A. H. Lu, E. L. Salabas and F. Schuth, *Angew. Chem., Int. Ed.*, 2007, **46**, 1222–1244.
- 15 R. K. Sharma, A. Puri, Y. Monga and A. Adholeya, *Sep. Purif. Technol.*, 2014, **127**, 121–130.
- 16 J. Zhang, S. Zhai, S. Li, Z. Xiao, Y. Song, Q. An and G. Tian, *Chem. Eng. J.*, 2013, **215–216**, 461–471.
- 17 Y. Ren, H. A. Abbood, F. He, H. Peng and K. Huang, *Chem. Eng. J.*, 2013, **226**, 300–311.
- 18 Y. Cui, J.-Q. Liu, Z.-J. Hu, X.-W. Xu and H.-W. Gao, *Anal. Methods*, 2012, **4**, 3095–3097.
- 19 B. Guo, F. Deng, Y. Zhao, X. Luo, S. Luo and C. Au, *Appl. Surf. Sci.*, 2014, **292**, 438–446.
- 20 R. Yi, G. Ye, D. Pan, F. Wu, M. Wen and J. Chen, *J. Mater. Chem. A*, 2014, **2**, 6840–6846.
- 21 R. K. Sharma, A. Puri, A. Kumar and A. Adholeya, *J. Environ. Sci.*, 2013, **25**, 1252–1261.
- 22 D. Ma, T. Veres, L. Clime, F. Normandin, J. Guan, D. Kingston and B. Simard, *J. Phys. Chem. C*, 2007, **111**, 1999–2007.

- 23 R. Abu-Reziq, H. Alper, D. Wang and M. L. Post, *J. Am. Chem. Soc.*, 2006, **28**, 5279–5282.
- 24 M. Yamaura, R. L. Camilo, L. C. Sampaio, M. A. Macedo, M. Nakamura and H. E. Toma, *J. Magn. Magn. Mater.*, 2004, **279**, 210–217.
- 25 V. S. Zaitsev, D. S. Filimonov, I. A. Presnyakov, R. J. Gambino and B. Chu, *J. Colloid Interface Sci.*, 1999, **212**, 49–57.
- 26 L. M. Rossi, F. P. Silva, L. L. R. Vono, P. K. Kiyohara, E. L. Duarte, R. Itri, R. Landers and G. Machado, *Green Chem.*, 2007, **9**, 379–385.
- 27 C. H. Weng, *J. Colloid Interface Sci.*, 2004, **272**(2), 262–270.
- 28 S. Yang, J. Hu, C. Chen, D. Shao and X. Wang, *Environ. Sci. Technol.*, 2011, **45**(8), 3621–3627.
- 29 P. Chand and Y. B. Pakade, *J. Chem.*, 2013, 164575.
- 30 M. Mohammadhosseini and M. S. Tehrani, *J. Chin. Chem. Soc.*, 2006, **53**, 1119–1128.
- 31 X. Jin, C. Yu, Y. Li, Y. Qi, L. Yang, G. Zhao and H. Hu, *J. Hazard. Mater.*, 2011, **186**, 1672–1680.
- 32 A. Kaur and U. Gupta, *J. Mater. Chem.*, 2009, **19**, 8279–8289.
- 33 Y. Wang, J. Xie, Y. Wu, H. Ge and X. Hu, *J. Mater. Chem. A*, 2013, **1**, 8782–8789.
- 34 A. Z. M. Badruddoza, Z. B. Z. Shawon, T. W. J. Daniel, K. Hidajat and M. S. Uddin, *Carbohydr. Polym.*, 2013, **91**, 322–332.
- 35 W. Liu, T. Wang, A. G. L. Borthwick, Y. Wang, X. Yin, X. Li and X. J. Ni, *Sci. Total Environ.*, 2013, **456–457**, 171–180.
- 36 P. Trivedi and L. Axe, *Environ. Sci. Technol.*, 2001, **35**, 1779–1784.
- 37 X. Ma, L. Li, L. Yang, C. Su, K. Wang, S. Yuan and J. Zhou, *J. Hazard. Mater.*, 2012, **209–210**, 467–477.
- 38 K. Inoue, K. Yoshizuka and K. Ohto, *Anal. Chim. Acta*, 1999, **388**, 209–218.
- 39 L. F. Koong, K. F. Lam, J. Barford and G. McKay, *J. Colloid Interface Sci.*, 2013, **395**, 230–240.
- 40 E. Repo, J. K. Warchoř, A. Bhatnagar, A. Mudhoo and M. Sillanpaa, *Water Res.*, 2013, **47**, 4812–4832.